## I. Amendment to the Claims

The following listing of the claims replaces all prior versions and listings of the claims in the application.

- (Previously Presented) A method of removing CO<sub>2</sub> from a gaseous stream comprising: contacting a gaseous stream with a solution, the solution being formed by combining at least:
  - a primary or secondary polyamine having an amine concentration of at least 4.0 equivalents/Kg water, wherein the amines located on the polyamine are not sterically hindered,
  - an alkali salt having a concentration of at least 1.0 equivalents/Kg water, and water:

wherein no monohydric or polyhydric alcohol is added to the solution; whereby contacting removes  $CO_2$  from the gaseous stream; and regenerating the solution.

- (Previously Presented) The method of claim 1, wherein the polyamine is piperazine, aminoethylpiperazine, hydroxyethylpiperazine, ethylenediamine, or dimethyl ethylenediamine.
- (Original) The method of claim 1, wherein the alkali salt is potassium carbonate, sodium carbonate, lithium carbonate, a bicarbonate salt, a bisulfide salt or a hydroxide salt.
- (Original) The method of claim 1, wherein the gaseous stream is contacted with the solution at a temperature of approximately 25°C.-120°C.
- (Previously Presented) The method of claim 1, wherein the rate constant for the reaction of CO<sub>2</sub> with the primary or secondary polyamine (K<sub>PZ</sub>) is at least 25 m<sup>3</sup>/mol-s at 25°C.
- 6. (Original) The method of claim 1, wherein the solution further comprises an additive.
- (Original) The method of claim 1, wherein the polyamine concentration and the alkali salt concentration are at least 2.3 m.

- (Original) The method of claim 1, wherein the ratio of equivalents of alkali salt to equivalents of polyamine is 0.3-3.0.
- (Original) The method of claim 1, further comprising applying a water wash system, wherein the water wash system collects the polyamine from treated gaseous stream.
- 10. (Original) The method of claim 1, wherein the rate for the solvent-mediated removal of CO<sub>2</sub> from the gaseous stream is at least 1.5 times the rate for CO<sub>2</sub> removal in a method using an aqueous solution of 5.0-M monoethanolamine.

## 11-16. (Canceled)

17. (Previously Presented) A method of removing CO<sub>2</sub> from a gaseous stream comprising: contacting a gaseous stream with a solution, the solution being formed by combining at least:

a primary or secondary polyamine having an amine concentration of at least 5.1 equivalents/Kg water, wherein the amines located on the polyamine are not sterically hindered,

an alkali salt having a concentration of at least 5.1 equivalents/Kg water, and water:

wherein no monohydric or polyhydric alcohol is added to the solution; whereby contacting removes CO<sub>2</sub> from the gaseous stream; and regenerating the solution.

- (Original) The method of claim 17, wherein the concentration of the polyamine and the concentration of the alkali salt are at least 5.5 equivalents/Kg water.
- (Original) The method of claim 17, wherein the concentration of the polyamine and the concentration of the alkali salt are approximately equal.
- (Previously Presented) The method of claim 17, wherein the polyamine is piperazine, aminoethylpiperazine, hydroxyethylpiperazine, ethylenediamine, or dimethyl ethylenediamine.

- (Original) The method of claim 17, wherein the alkali salt is potassium carbonate, sodium carbonate, lithium carbonate, a bicarbonate salt, a bisulfide salt or a hydroxide salt.
- (Original) The method of claim 17, wherein the gaseous stream is contacted with the solution at a temperature of approximately 25°C-120°C.
- (Previously Presented) The method of claim 17, wherein the rate constant for the reaction of CO<sub>2</sub> with the primary or secondary polyamine (K<sub>PZ</sub>) is at least 25 m<sup>3</sup>/mol-s at 25°C.
- 24. (Original) The method of claim 17, wherein the solution further comprises an additive.
- 25. (Original) The method of claim 17, wherein the rate for the solvent-mediated removal of CO<sub>2</sub> from the gaseous stream is at least 1.5 times the rate for CO<sub>2</sub> removal in a method using an aqueous solution of 5.0-M monoethanolamine.
- 26. (Previously Presented) A method of removing CO<sub>2</sub> from a gaseous stream comprising: contacting a gaseous stream with a solution, the solution being formed by combining at least:
  - a primary or secondary polyamine having an amine concentration of at least 4.0 equivalents/Kg water, wherein the amines located on the polyamine are not sterically hindered,
  - an alkali salt having a concentration of at least 1.0 equivalents/Kg water, and water;

wherein no monohydric or polyhydric alcohol is added to the solution; whereby contacting removes  ${\rm CO_2}$  from the gaseous stream; and regenerating the solution.

## (Canceled)

 (Previously Presented) The method of claim 26, wherein the polyamine is piperazine, aminoethylpiperazine, hydroxyethylpiperazine, ethylenediamine, or dimethyl ethylenediamine.

- (Original) The method of claim 26, wherein the alkali salt is potassium carbonate, sodium carbonate, lithium carbonate, bicarbonate salt, a bisulfide salt, or a hydroxide salt.
- (Original) The method of claim 26, wherein the gaseous stream is contacted with the solution at a temperature of approximately 25°C-120°C.
- (Previously Presented) The method of claim 26, wherein the rate constant for the reaction of CO<sub>2</sub> with the primary or secondary polyamine (K<sub>PZ</sub>) is at least 25 m<sup>3</sup>/mol-s at 25°C.
- 32. (Original) The method of claim 26, wherein the solution further comprises an additive.
- (Original) The method of claim 26, wherein the polyamine concentration and the alkali salt concentration are at least 2.3 m.
- (Original) The method of claim 26, wherein the ratio of equivalents of alkali salt to equivalents of polyamine is 0.3-3.0.
- 35. (Original) The method of claim 26, wherein the rate for the solvent-mediated removal of CO<sub>2</sub> from the gaseous stream is at least 1.5 times the rate for CO<sub>2</sub> removal in a method using an aqueous solution of 5.0-M monoethanolamine.
- 36. (Currently Amended) A method of removing CO<sub>2</sub> from a gaseous stream comprising: contacting a gaseous stream with a solution, the solution being formed by combining at least.
  - a piperazine derivative having an amine concentration of 4.0-10.0 equivalents/Kg water, wherein the amines located on the piperazine derivative are not sterically hindered.
  - an alkali salt having a concentration of  $\frac{3.0-10.0}{4.0-10.0}$  equivalents/Kg water, and

water;

wherein the concentration of the piperazine derivative and the concentration of the alkali salt are approximately equal;

wherein no monohydric or polyhydric alcohol is added to the solution;

- whereby contacting removes CO<sub>2</sub> from the gaseous stream; and regenerating the solution.
- (Previously Presented) The method of claim 36, wherein the piperazine derivative is piperazine, aminoethylpiperazine, or hydroxyethylpiperazine.
- (Original) The method of claim 36, wherein the alkali salt is potassium carbonate, sodium carbonate, lithium carbonate, a bicarbonate salt, a bisulfide salt, or a hydroxide salt.
- (Original) The method of claim 36, wherein the gaseous stream is contacted with the solution at a temperature of approximately 25°C-120°C.
- (Original) The method of claim 36, wherein the rate constant for the reaction of CO<sub>2</sub> with the piperazine derivative (K<sub>FZ</sub>) is at least 25 m<sup>3</sup>/mol-s at 25°C.
- 41. (Original) The method of claim 36, wherein the solution further comprises an additive.
- 42. (Original) The method of claim 36, wherein the rate for the solvent-mediated removal of CO<sub>2</sub> from the gaseous stream is at least 1.5 times the rate for CO<sub>2</sub> removal in a method using an aqueous solution of 5.0-M monoethanolamine.